

# Simulation of Lean Premixed Turbulent Combustion

J. Bell

Lawrence Berkeley National Laboratory

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Collaborators: M. Day, J. Grcar, V. Beckner, M. Lijewski  
R. Cheng, M. Johnson, I. Shepherd,  
S. Tachibana



# Lean Premixed Turbulent Combustion



Rod-stabilized  
V-flame



4-jet Low-swirl burner  
(LSB)



Slot burner

- Potential for efficient, low-emission power systems
- Design issues because of flame instabilities
- Limitations of theory and experiment
- Can we safely and reliably burn hydrogen for power generation?

# Basic Physics of Combustion

Focus on gas phase combustion

Fluid mechanics

- Conservation of mass
- Conservation of momentum
- Conservation of energy

Thermodynamics

- Pressure, density, temperature relationships for multicomponent mixtures

Chemistry

- Reaction kinetics

Species transport

- Diffusive transport of different chemical species within the flame

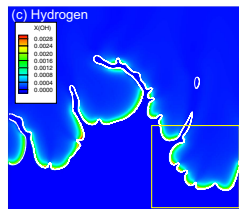
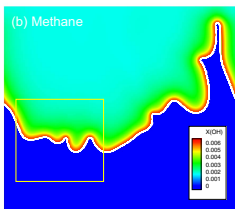
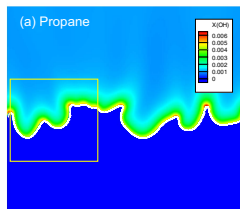
Radiation

- Energy emission by hot gases

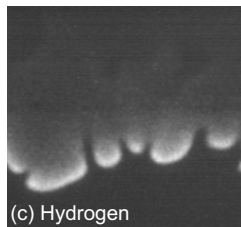
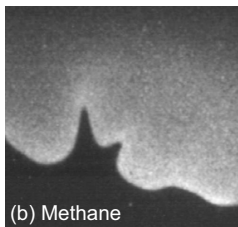
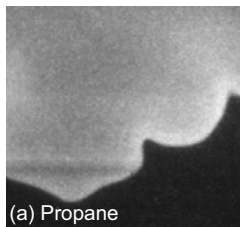
Low-swirl burner



# Fuel dependence of flame structure



OH Mole fraction



OH PLIF

# Compressible Navier Stokes

Gas phase combustion – mixture model for diffusion

$$\text{Mass} \quad \rho_t + \nabla \cdot \rho \mathbf{U} = 0$$

$$\text{Momentum} \quad (\rho \mathbf{U})_t + \nabla \cdot (\rho \mathbf{U} \mathbf{U} + \mathbf{p}) = \rho \vec{g} + \nabla \cdot \boldsymbol{\tau}$$

$$\text{Energy} \quad (\rho E)_t + \nabla \cdot (\rho \mathbf{U} E + \mathbf{p} \mathbf{U}) = \nabla \cdot \kappa \nabla T + \nabla \cdot \boldsymbol{\tau} \mathbf{U} \\ + \sum_m \nabla \cdot (\rho h_m D_m \nabla Y_m)$$

$$\text{Species} \quad (\rho Y_m)_t + \nabla \cdot (\rho \mathbf{U} Y_m) = \nabla \cdot (\rho D_m \nabla Y_m) + \dot{\omega}_m$$

Augmented with

- Thermodynamics
- Reaction kinetics
- Transport coefficients

Need to preserve chemical and transport fidelity



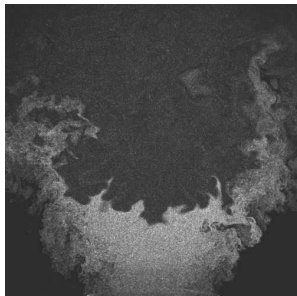
## Spatial Scales

- Domain:  $\approx 10$  cm
- Flame thickness:  $\delta_T \approx 1$  mm
- Integral scale:  $l_t \approx 2 - 6$  mm

## Temporal Scales

- Flame speed  $O(10^2)$  cm/s
- Mean Flow:  $O(10^3)$  cm/s
- Acoustic Speed:  $O(10^5)$  cm/s

Wide range of length and time scales will make this computationally demanding



Mie Scattering Image

## Simulation requirements

- No explicit model for turbulence, or turbulence/chemistry interactions
- Detailed chemistry based on fundamental reactions, detailed diffusion
- “Sufficient” range of scales to represent realistic flames

## Simulation issues

- Wide range of length and time scale
- Multiple physical processes
- Complex state description
- Exploit high-performance architectures

Consider different approaches to attacking this problem



# Computational strategies

**Scaling is paramount:** Low communication, explicit discretizations, balanced work load – let the machine do the work

- Generic mathematical model
- Define spatial discretization – structured, unstructured, adaptive
- Identify time step based on stability requirements
- Integrate with explicit ODE algorithm
- Range of time scales determines performance

**Coupling is paramount:** Fully implicit, method of lines, iterative algorithms – preconditioners do the work

- Generic mathematical model
- Define spatial discretization – structured, unstructured, adaptive
- Identify time step based on accuracy requirements
- Integrate with implicit ODE algorithm
- Efficiency of solver/preconditioner determines performance





**Mathematical structure is paramount:** Develop customized algorithms for specific problem classes. Exploit mathematical structure to compute more efficiently

Components of a computational model

- Mathematical model: describe the problem in a way that is amenable to representation in a computer simulation
- Approximation / discretization: approximate the mathematical model with a finite number of degrees of freedom
- Solvers and software: develop algorithms for solving the discrete approximation efficiently on high-end architecture

**To fundamentally change the way we solve these types of problems, we need to consider each of these components and how they fit together**



# Mathematical formulation

Exploit natural separation of scales between fluid motion and acoustic wave propagation

Low Mach number model,  $M = U/c \ll 1$  (Rehm & Baum 1978, Majda & Sethian 1985)

Start with the compressible Navier-Stokes equations for multicomponent reacting flow, and expand in the Mach number,  $M = U/c$ .

Asymptotic analysis shows that:

$$p(\vec{x}, t) = p_0(t) + \pi(\vec{x}, t) \quad \text{where} \quad \pi/p_0 \sim \mathcal{O}(M^2)$$

- $p_0$  does not affect local dynamics,  $\pi$  does not affect thermodynamics
- For open containers  $p_0$  is constant
- Pressure field is instantaneously equilibrated – removed acoustic wave propagation



# Low Mach number equations

$$\text{Momentum} \quad \rho \frac{DU}{Dt} = -\nabla \pi + \nabla \cdot \left[ \mu \left( \frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} - \frac{2}{3} \delta_{ij} \nabla \cdot \mathbf{U} \right) \right]$$

$$\text{Species} \quad \frac{\partial(\rho Y_m)}{\partial t} + \nabla \cdot (\rho \mathbf{U} Y_m) = \nabla \cdot (\rho \mathbf{D}_m \nabla Y_m) + \dot{\omega}_m$$

$$\text{Mass} \quad \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{U}) = 0$$

$$\text{Energy} \quad \frac{\partial \rho h}{\partial t} + \nabla \cdot (\rho h \vec{\mathbf{U}}) = \nabla \cdot (\lambda \nabla T) + \sum_m \nabla \cdot (\rho h_m \mathbf{D}_m \nabla Y_m)$$

Equation of state  $\rho_0 = \rho \mathcal{R} T \sum_m \frac{Y_m}{W_m}$  constrains the evolution

System contains evolution equations for  $U$ ,  $Y_m$ ,  $\rho$ ,  $h$ , with a constraint.

Low Mach number system can be advanced at fluid time scale instead of acoustic time scale but . . .

**We need effective integration techniques for this more complex formulation**



# Constraint for reacting flows

Low Mach number system is a system of PDE's evolving subject to a constraint; differential algebraic equation (DAE) with index 3

Differentiate constraint to reduce index

Here, we differentiate the EOS along particle paths and use the evolution equations for  $\rho$  and  $T$  to define a constraint on the velocity:

$$\begin{aligned}\nabla \cdot U &= \frac{1}{\rho} \frac{D\rho}{Dt} = -\frac{1}{T} \frac{DT}{Dt} - \frac{\mathcal{R}}{R} \sum_m \frac{1}{W_m} \frac{DY_m}{Dt} \\ &= \frac{1}{\rho c_p T} \left( \nabla \cdot (\lambda \nabla T) + \sum_m \rho D_m \nabla Y_m \cdot \nabla h_m \right) + \\ &\quad \frac{1}{\rho} \sum_m \frac{W}{W_m} \nabla (D_m \rho \nabla Y_m) + \frac{1}{\rho} \sum_m \left( \frac{W}{W_m} - \frac{h_m(T)}{c_p T} \right) \omega_m \\ &\equiv S\end{aligned}$$



# Incompressible Navier Stokes Equations

For iso-thermal, single fluid systems this analysis leads to the incompressible Navier Stokes equations

$$U_t + U \cdot \nabla U + \nabla \pi = \mu \Delta U$$

$$\nabla \cdot U = 0$$

How do we develop efficient integration schemes for this type of constrained evolution system?

Vector field decomposition

$$V = U_d + \nabla \phi$$

where  $\nabla \cdot U_d = 0$

and

$$\int U \cdot \nabla \phi dx = 0$$

We can define a projection  $\mathbf{P}$

$$\mathbf{P} = I - \nabla(\Delta^{-1})\nabla \cdot$$

such that  $U_d = \mathbf{P}V$

Solve  $-\Delta \phi = \nabla \cdot V$

Then  $U_t = \mathbf{P}(\mu \Delta U - U \cdot \nabla U)$



Incompressible Navier Stokes equations

$$U_t + U \cdot \nabla U + \nabla \pi = \mu \Delta U$$

$$\nabla \cdot U = 0$$

Advection step

$$\frac{U^* - U^n}{\Delta t} + U \cdot \nabla U = \frac{\mu}{2} \Delta (U^* + U^n) - \nabla \pi^{n-1/2}$$

Projection step

$$U^{n+1} = \mathbf{P}U^*$$

Can we use this for LMC model?

- Finite amplitude density variation
- inhomogenous constraint

# Variable coefficient projection

Generalized vector field decomposition

$$V = U_d + \frac{1}{\rho} \nabla \phi$$

where  $\nabla \cdot U_d = 0$  and  $U_d \cdot n = 0$  on the boundary

Then  $U_d$  and  $\frac{1}{\rho} \nabla \phi$  are orthogonal in a density weighted space.

$$\int \frac{1}{\rho} \nabla \phi \cdot U \rho \, dx = 0$$

Defines a projection  $\mathbf{P}_\rho = I - \frac{1}{\rho} \nabla ((\nabla \cdot \frac{1}{\rho} \nabla)^{-1}) \nabla \cdot$  such that  $\mathbf{P}_\rho V = U_d$ .

$\mathbf{P}_\rho$  is idempotent and  $\|\mathbf{P}_\rho\| = 1$



# Generalized vector field decomposition

Use variable- $\rho$  projection to define a generalized vector field decomposition

$$\mathbf{V} = \mathbf{U}_d + \nabla\xi + \frac{1}{\rho}\nabla\phi$$

where

$$\nabla \cdot \nabla\xi = S$$

and

$$\nabla \cdot \mathbf{U}_d = 0$$

We can then define

$$\mathbf{U} = \mathbf{P}_\rho(\mathbf{V} - \nabla\xi) + \nabla\xi$$

so that  $\nabla \cdot \mathbf{U} = S$  with  $\mathbf{P}_\rho(\frac{1}{\rho}\nabla\phi) = 0$

- This construct allows us to define a projection algorithm for variable density flows with inhomogeneous constraints
- Requires solution of a variable coefficient elliptic PDE
- Allows us to write system as a pure initial value problem





# Low Mach number algorithm

Numerical approach based on generalized vector field decomposition  
Fractional step scheme

- Advance velocity and thermodynamic variables
  - Advection
  - Diffusion
  - Stiff reactions
- Project solution back onto constraint

Stiff kinetics relative to fluid dynamical time scales

$$\frac{\partial(\rho Y_m)}{\partial t} + \nabla \cdot (\rho \mathbf{U} Y_m) = \nabla \cdot (\rho \mathbf{D}_m \nabla Y_m) + \dot{\omega}_m$$

$$\frac{\partial(\rho h)}{\partial t} + \nabla \cdot (\rho \mathbf{U} h) = \nabla \cdot (\lambda \nabla T) + \sum_m \nabla \cdot (\rho h_m \mathbf{D}_m \nabla Y_m)$$

Operator split approach

- Chemistry  $\Rightarrow \Delta t/2$
- Advection – Diffusion  $\Rightarrow \Delta t$
- Chemistry  $\Rightarrow \Delta t/2$

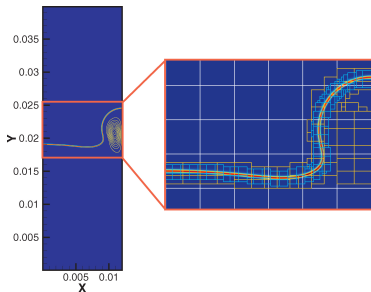


AMR – exploit varying resolution requirements in space and time  
 Block-structured hierarchical grids

- Amortize irregular work

Each grid patch (2D or 3D)

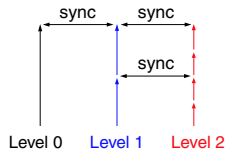
- Logically structured, rectangular
- Refined in space and time by evenly dividing coarse grid cells
- Dynamically created/destroyed



2D adaptive grid hierarchy

Subcycling:

- Advance level  $l$ , then
  - Advance level  $l + 1$   
 level  $l$  supplies boundary data
  - Synchronize levels  $l$  and  $l + 1$



# AMR Synchronization

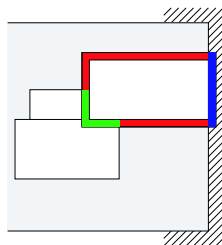
Coarse grid supplies Dirichlet data as boundary conditions for the fine grids.

Errors take the form of flux mismatches at the coarse/fine interface.

Design Principles:

- Define what is meant by the solution on the grid hierarchy.
- Identify the errors that result from solving the equations on each level of the hierarchy “independently”.
- Solve correction equation(s) to “fix” the solution.
- Correction equations match the structure of the process they are correcting.

- Fine-Fine
- Physical BC
- Coarse-Fine



*Preserves properties of single-grid algorithm*

## Complex multiphysics application

- Advective transport – hyperbolic
- Diffusive transport – nonlinear parabolic systems
- Projections – variable coefficient elliptic equations
- Chemical kinetics – stiff ODE's

## Dynamic adaptive refinement

Computation requires high-performance parallel architectures

## Need to manage software complexity

- Develop data abstractions to support AMR algorithms
- Support parallelization strategy: Distribute grid patches to processors
- Encapsulate data / parallelization in reusable software framework



## BoxLib foundation library:

- Domain specific class library: supports solution of PDE's on hierarchical structured adaptive grid
- Functionality for serial, distributed memory & shared memory parallel architectures
  - MPI communication
  - Programming interface through loop iteration constructs

## AMR framework library:

- Flow control, memory management, grid generation, checkpoint/restart and plotfile generation

## Key issues in parallel implementation

- Dynamic load balancing
- Optimizing communication patterns
- Efficient manipulation of metadata
- Fast linear solvers



Does all of this machinery buy us anything?

Folklore (urban legend) says “Since complicated AMR algorithms don’t scale, can’t I solve my problem faster with a scalable algorithm on a machine with a lot of processors?”

How well do these algorithms scale? What is the implication for solving hard problems?

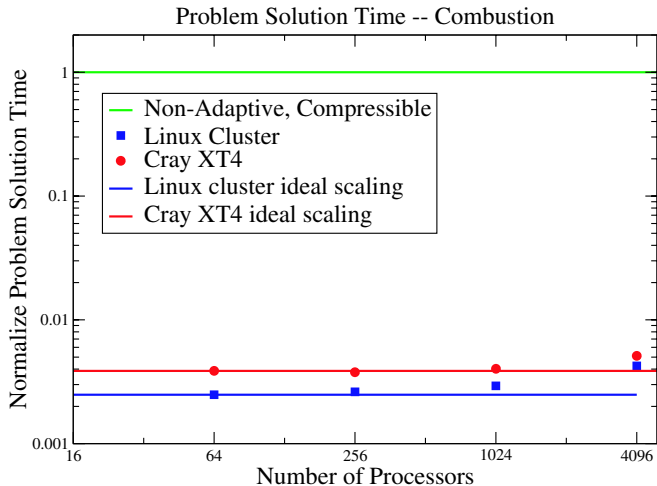
Weak scaling

- Let problem get larger as we increase number of processors
- Constant work per processor
- Tests full algorithm
- AMR neutral – fraction of domain refined is invariant

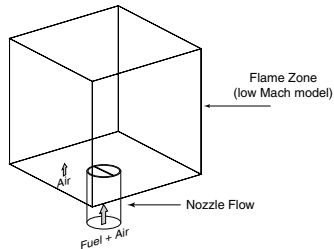
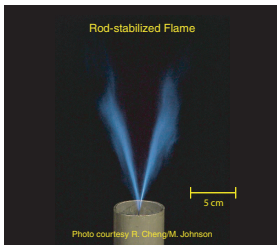
Compare to explicit non-adaptive CNS solver



# LMC Performance – Methane Flame



# V-flame Validation



Strategy - Treat nozzle exit as inflow boundary condition for combustion simulation

Problem specification

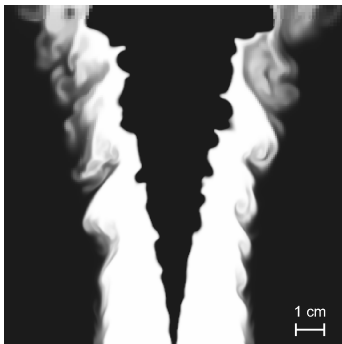
- 12cm x 12cm x 12cm domain
- DRM-19: 20 species, 84 reactions

Inflow characteristics

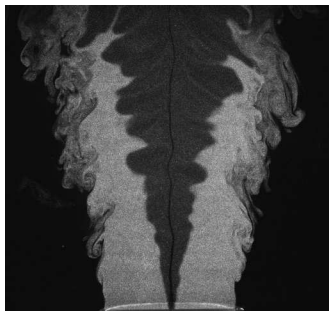
- Mean flow
  - 3 m/s mean inflow
  - Boundary layer profile at edge
  - Noflow condition to model rod
  - Weak co-flow air
- Turbulent fluctuations
  - $\ell_t = 3.5\text{mm}$ ,  $u' = 0.18\text{m/sec}$
  - Estimated  $\eta = 220\mu\text{m}$



# Results: Computation vs. Experiment

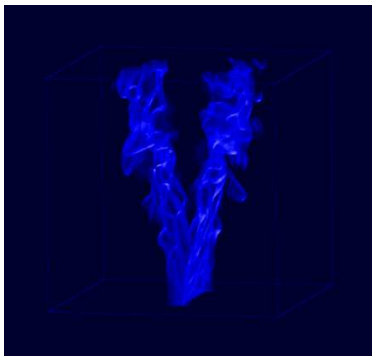


$CH_4$  from simulation

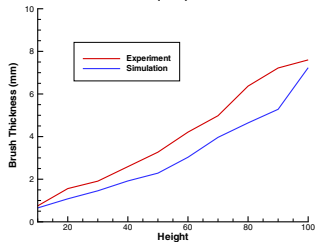
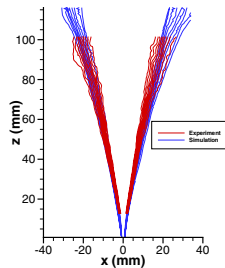


Single image from  
experimental PIV

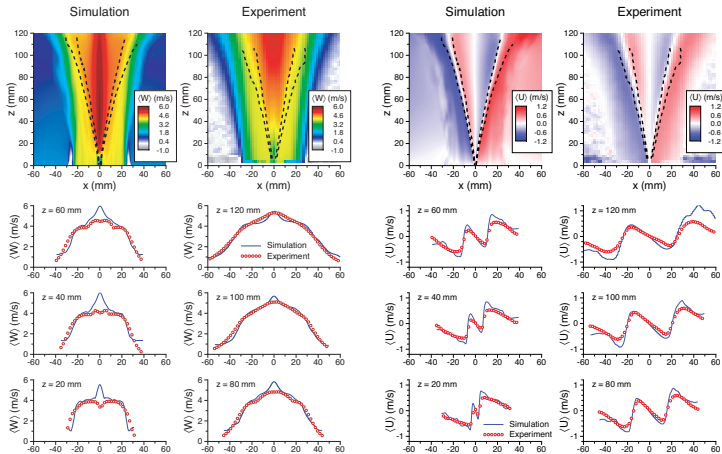
# Flame Surface



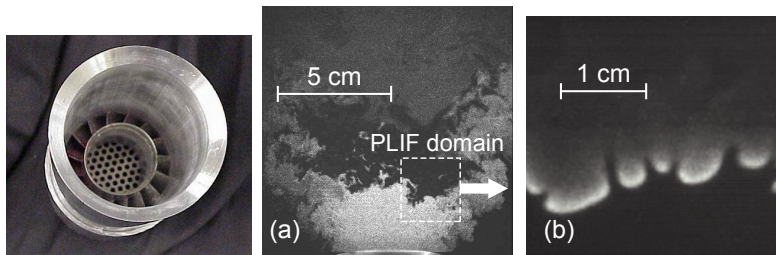
Instantaneous flame surface



# Velocity comparison



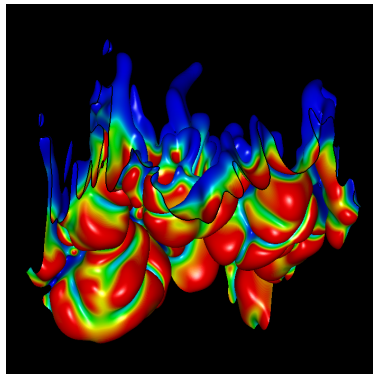
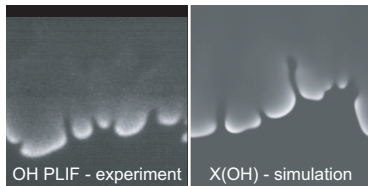
# Hydrogen combustion



- OH PLIF shows gaps in the flame
- How do these flames burn?
- Are existing engineering models applicable?
- Can standard flame analysis techniques be used to analyze structure?

# Hydrogen flame in 3D

3D control simulation of detailed hydrogen flame at laboratory scales  
( $3 \times 3 \times 9$  cm domain,  $\Delta x_f = 58 \mu\text{m}$ )

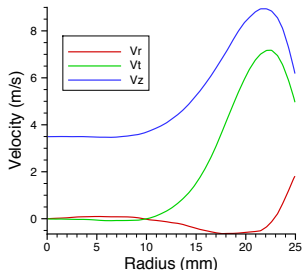


- Figure is “underside”  
(from fuel side of flame)
- Flame surface (isotherm)  
colored by local fuel  
consumption
- Cellular structures convex  
to fuel, robust extinction  
ridges

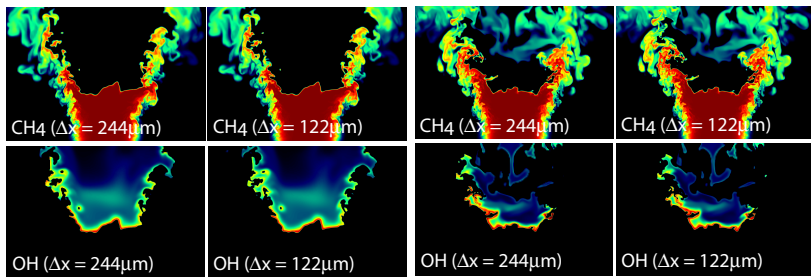
# Low swirl burner simulations

## Strategy:

- Treat outflow from the nozzle as an inflow boundary condition
  - Mean flow and turbulent intensities from measured data
  - Impose synthetic turbulence as a perturbation to mean inflow
- Simulate flow in a rectilinear domain sitting above the outflow
- Four cases
  - Hydrogen ( $\phi = 0.37$ ) and methane ( $\phi = 0.7$ )
  - Laminar flame speed approximately 15 cm / sec
  - Two levels of mean flow and turbulence



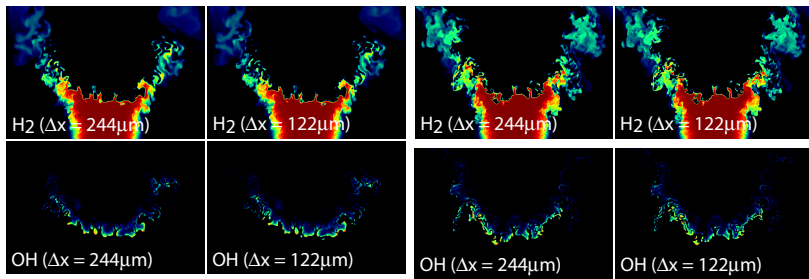
# Methane swirl simulations



Weak Turbulence

Strong Turbulence

# Hydrogen swirl simulations

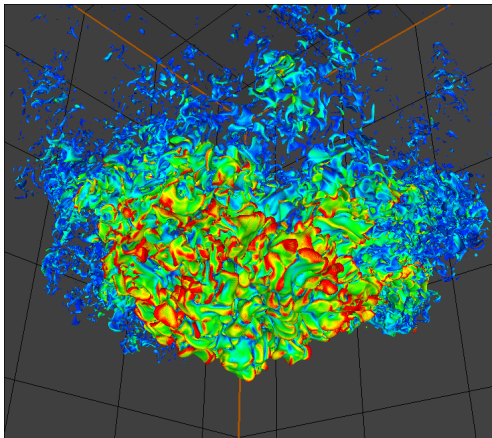


Weak Turbulence

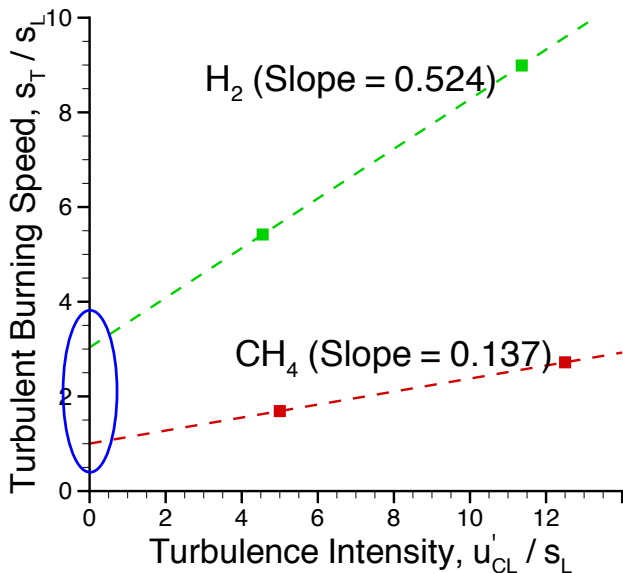
Strong Turbulence



# Hydrogen flame surface



# Flame Speeds



Developed new methodology to simulate realistic turbulent flames based on exploiting mathematical structure of combustion problems

Consider all aspects of the problem

- Low Mach number formulation – models
- Projection-based integration methodology – algorithms
- Adaptive mesh refinement – algorithms
- Parallel software infrastructure – solvers and software

There is a tension between these different elements

Algorithms reflect mathematical properties of the problem:  
Analysis based discretization



Combining all of these elements resulted in several orders of magnitude improvement in performance, enabling simulations of laboratory-scale premixed turbulent flames with:

- Detailed chemistry and transport
- No explicit models for turbulence or turbulence / chemistry interaction

Future work

- Improved characterization of turbulence conditions
- Closed chamber simulations with long wavelength acoustics
- Include nitrogen chemistry for emissions
- High-pressure simulations

